AMENDMENTS TO THE CLAIMS

1. (Currently Amended) Method of purifying an antibody, ~~preferably an IgG antibody,~~ comprising the steps of:
    1. Purifying an antibody by means of protein A affinity chromatography wherein the protein A is a native protein A or a functional derivative thereof,
    2. loading the thus purified antibody comprising antibody aggregate and protein A or protein A derivative onto an ion ~~exchange~~exchanger ~~material~~ under conditions which allow of binding of the contaminating protein A or its functional derivative to the ion exchanger ~~material~~ and which conditions further allow of resolution in the flow-through of antibody aggregates from antibody monomer which monomer is not complexed with protein A or protein A derivative ~~by means of fractionation of the flow-through,~~ and further
    3. fractionating the flow-through of step 2) and harvesting from the flow-through ~~of the ion exchanger~~ at least one antibody monomer fraction having both reduced contents of protein A or protein A derivative and further reduced contents of antibody aggregate as compared to the composition of antibody as loaded onto the ion ~~exchange~~exchanger ~~material~~ before by fractionating or splitting the antibody peak of the flow-through into at least two fractions and wasting the tail fraction.

2. (Previously Presented) Method according to claim 1, characterized in that the protein A is a recombinant protein A that is engineered such as to allow of single-point attachment to a column material.

3. (Original) Method according to claim 2, characterized in that the recombinant protein A comprises a cysteine in its amino acid sequence.

4. (Original) Method according to claim 3, characterized in that the cysteine is comprised in a segment that consists of the last 30 Amino acids of the C-terminus of the amino acid sequence of the recombinant protein A.

5. (Cancelled)

6. (Currently Amended) Method according to claim ~~3~~1, characterized in that the protein A or its functional derivative is reduced to a concentration of <1ng/mg IgG in the flow-through of the ion exchanger.

7. (Currently Amended) Method according to claim ~~3~~1, characterized in that the monomericity of the antibody harvested is at least 99%~~ and is achieved by fractionating the antibody peak of the flow-through into at least two fractions and wasting the tail fraction~~.

8. (Currently Amended) Method according to claim ~~3~~1, characterized in that the antibody is a monoclonal antibody~~, preferably an IgG antibody wherein the IgG antibody may be chimeric or CDR-grafted IgG antibody~~.

9. (Currently Amended) Method according to claim ~~3~~1, characterized in that the antibody is harvested from a cell culture prior to purifying the antibody by means of protein A affinity chromatography.

10. (Currently Amended) Method according to claim ~~3~~1, characterized in that the antibody is harvested from a mammalian cell culture.

11. (Currently Amended) Method according to claim ~~3~~1, characterized in that the antibody that is to be purified by means of protein A affinity chromatography is not treated as to inactivate proteases~~, preferably is not in admixture with at least one protease inhibitor~~.

12. (Cancelled)

13. (Currently Amended) Method of purifying a product protein, comprising the steps of:
    1. loading a solution comprising product protein which product protein comprises ~~monoleric~~ monomeric and aggregated forms of said protein onto an ion ~~exchange~~exchanger ~~material~~ under conditions which allow of resolution in the ~~flow-through~~flow-through of said

product protein aggregates from said product protein monomer which monomer ~~preferably~~ is not further complexed with a second protein ligand, ~~by means of fractionation of the flow-through~~ and further

2. fractionating the flow-through of step 1) and harvesting from the flow-through ~~of the ion exchanger~~ at least one product protein monomer fraction having reduced contents of product protein aggregate as compared to the composition of product protein loaded onto the ion ~~exchange~~exchanger ~~material~~ for purification by fractionating or splitting the product protein peak of the flow-through into at least two fractions and wasting the tail fraction.

14-15. (Cancelled)

16. (Currently Amended) Method according to claim ~~15~~1, characterized in that at least one buffer is used for loading and rinsing the ion exchanger which at least one buffer coming off the ion exchanger is constituting the flow-through comprising the product protein peak.

17. (Currently Amended) Method according to claim 16, characterized in that the pH of said buffer is set at a pH which is the ~~pi~~pI or average ~~pi~~pI of the product protein monomer sought to be purified in the range of ±0.5 pH units around said ~~pi~~pI.

18. (Currently Amended) Method according to claim 16, characterized in that the pH of said buffer is set at a pH different from the ~~pi~~pI or average ~~pi~~pI of the product protein monomer sought to be purified and which pH further vests the product protein monomer with a surface charge which charge leads to ionic attraction in between product protein monomer and the charged groups of the ion ~~exchange~~exchanger ~~material~~ when exposed to or submerged in said buffer.

19. (Currently Amended) Method according to claim 18, characterized in that in case of a cation exchanger, the pH of the buffer is set at a value below the average ~~pi~~pI of the product protein monomer sought to be purified~~, preferably set at a value of from 0.5 to 3 pH units below said average pi~~.

20. (Currently Amended) Method according to claim 18, characterized in that in case of an anion exchanger, the pH of the buffer is set at a value above the average ~~pi~~pI of the product protein monomer sought to be purified~~, preferably set at a value of from 0.5 to 3 pH units above said average pi~~.

21. (Currently Amended) Method according to claim 13, characterized in that said conditions are non-binding conditions as regards binding of the product protein monomer to the ion exchanger ~~material~~ such as that consequently more than 70% (w/w)~~-~~, ~~more preferably more than 80% (w/w)~~ of the product protein loaded onto the ion ~~exchange~~exchanger ~~material~~ can be recovered in the flow-through from the ion ~~exchange~~exchanger ~~material~~.

22. (Cancelled)

23. (New) Method according to claim 8, characterized in that the monoclonal antibody is an IgG antibody wherein the IgG antibody may be chimeric or CDR-grafted IgG antibody.

24. (New) Method according to claim 23 above, characterized in that the IgG antibody is a chimeric or a CDR-grafted IgG antibody.

25. (New) Method according to claim 19, wherein the pH of the buffer is set at a value of from 0.5 to 3 pH units below said average pI.

26. (New) Method according to claim 20, wherein the pH of the buffer is set at a value of from 0.5 to 3 pH units above said average pI.